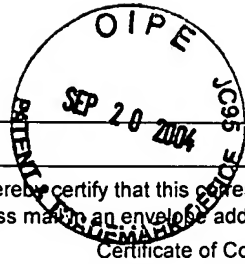


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**OFFICIAL**

CERTIFICATE OF MAILING			
I hereby certify that this correspondence is being deposited with the United States Postal Service with sufficient postage as first class mail in an envelope addressed to: Certificate of Correction Branch, Commissioner for Patents, P.O. Box 1450, Alexandria, VA 22313-1450			
Name (Print/Type)	Rose A. Lubich		
Signature	<i>Rose A. Lubich</i>	Date	9-16-04

**PATENT**

**IN THE UNITED STATES PATENT AND TRADEMARK OFFICE**

Patent No.: 6,790,802 B1

Issued: 09/14/2004

Inventor(s): Paul A. Sechrist

Title: CYCLIC CATALYST REGENERATION PROCESS USING ADSORPTION AND DESORPTION ON VENT STREAM

**REQUEST FOR CERTIFICATE OF CORRECTION OF PATENT FOR PTO MISTAKE (37 CFR 1.322(a))**

Certificate of Correction Branch  
Commissioner for Patents  
P.O. Box 1450  
Alexandria, VA 22313-1450

Sir:

The above-designated patent issued with the following errors.

**In claim 21:** In column 16, line 45, immediately following "formed," insert "from".

In accord with the requirements of the "Expedited Issuance of Certificates of Correction When the Error is Attributable to the United States Patent and Trademark Office" (Official Gazette, September 17, 2002), Patentee encloses a copy of the claims from the subject application (Appl. No. 10/007,853) which was filed on November 5, 2001, in which the subject claim appears correctly. No amendments were made to the application.

It is believed that the enclosed documentation unequivocally supports Patentee's assertion that the error incurred through the fault of the PTO. Therefore, the requirements for expedited issuance of the Certificate of Correction are met.

Attached is Form PTO-1050. It is believed that no fee is required.

Respectfully submitted,

LOP LLC

*Michael A. Moore*

Michael A. Moore

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MAM:sb

**Certificate**  
**SEP 23 2004**  
**of Correction**

**23 SEP 2004**

**UNITED STATES PATENT AND TRADEMARK OFFICE  
CERTIFICATE OF CORRECTION**

PATENT NO.: 6,790,802 B1  
DATED: 09/14/2004  
INVENTOR: Paul A. Sechrist

It is certified that error appears in the above-identified patent and that said Letters Patent is hereby corrected as shown below:

The above-designated patent issued with the following error:

In claim 21: In column 16, line 45, immediately following "formed," insert "from".

MAILING ADDRESS OF SENDER:

JOHN G. TOLOMEI  
UOP LLC  
25 EAST ALGONQUIN ROAD  
DES PLAINES, ILLINOIS 60017-5017

PATENT NO. 6,790,802 B1

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23 SEP 2004

**UNITED STATES PATENT AND TRADEMARK OFFICE  
CERTIFICATE OF CORRECTION**

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INVENTOR: Paul A. Sechrist

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WE CLAIM:

1. A process for the regeneration of a hydrocarbon conversion catalyst in the presence of a halogen-containing material, the process comprising:

- 5 (a) contacting a regeneration inlet stream comprising a first component selected from the group consisting of oxygen, hydrogen, nitrogen, and a C<sub>1</sub>-C<sub>5</sub> hydrocarbon with a catalyst in the presence of a halogen-containing material at regeneration conditions to at least partially regenerate said catalyst and produce a regeneration effluent stream comprising said material and said first component;
- 10 (b) contacting a first portion of said regeneration effluent stream with an adsorbent, adsorbing said material on said adsorbent at adsorption conditions, and recovering an adsorption effluent stream comprising said first component and having a reduced concentration of said material relative to said first portion of said regeneration effluent stream;
- 15 (c) contacting a desorption inlet stream comprising a second component selected from the group consisting of oxygen, hydrogen, nitrogen, and a C<sub>1</sub>-C<sub>5</sub> hydrocarbon with said adsorbent, said adsorbent having said material adsorbed thereon, desorbing said material from said adsorbent at desorption conditions, and recovering a desorption effluent stream comprising said material and said
- 20 second component; and,
- (d) forming said regeneration inlet stream from a second portion of said regeneration effluent stream and at least a portion of said desorption effluent stream.

25 2. The process of Claim 1 wherein said adsorbent is selected from the group consisting of a molecular sieve, silica gel, carbon, and alumina.

3. The process of Claim 1 wherein said catalyst is selected from the group consisting of a reforming catalyst, an isomerization catalyst, and a dehydrogenation catalyst.

4. The process of Claim 1 wherein said regeneration is selected from the group consisting of burning carbon deposits on said catalyst, redispersing a metal on said catalyst, adding halogen to said catalyst, drying said catalyst, and reducing a metal on said catalyst.
- 5 5. The process of Claim 1 further characterized in that at least about 80 percent of said material in said regeneration effluent stream is adsorbed on said adsorbent.
6. The process of Claim 1 further characterized in that at least about 90 percent of said material in said regeneration effluent stream is adsorbed on said adsorbent.
7. The process of Claim 1 further characterized in that said adsorption conditions  
10 comprise a temperature of less than about 482°C and a molar ratio of water to halogen of more than 5:1.
8. The process of Claim 1 further characterized in that said adsorbent has a capillary condensation temperature at said adsorption conditions, and said adsorption conditions comprise a temperature of greater than said capillary condensation  
15 temperature.
9. The process of Claim 1 wherein said halogen is chlorine or fluorine.
10. The process of Claim 1 wherein said material is selected from the group consisting of hydrogen chloride and molecular chlorine.
11. The process of Claim 1 further characterized in that said adsorbent has a pre-  
20 adsorption halogen content prior to said contacting and said adsorbing in (b), said adsorbent has a post-adsorption halogen content after said contacting and said desorbing in (c), and the difference between said pre-adsorption halogen content and said post-adsorption halogen content is from about 0.2 to about 2.0 wt-% halogen, based on the weight of the adsorbent.
- 25 12. The process of Claim 1 further characterized in that said regeneration inlet stream has a regeneration inlet temperature and a regeneration inlet molar ratio of water to halogen, said desorption effluent stream has a desorption effluent temperature and a desorption effluent molar ratio of water to halogen, the difference between said regeneration inlet temperature and said desorption effluent temperature is less than

about 20°C, and the difference between said regeneration inlet molar ratio and said desorption effluent molar ratio is less than about 5:1.

13. The process of Claim 1 further characterized in that the adsorption conditions comprise an adsorption temperature and an adsorption molar ratio of water to halogen, the desorption conditions comprise a desorption temperature and a desorption molar ratio of water to halogen, the difference between the desorption temperature and the adsorption temperature is more than about 55°C, and the ratio of the adsorption molar ratio to the desorption molar ratio is from about 0 to about 2.

14. The process of Claim 1 further characterized in that a component consisting of at least one of water and a compound that can react to form water is introduced into said process and said water contacts said adsorbent in (c).

15. The process of Claim 1 further characterized in that at least one of said second portion of said regeneration effluent stream, said at least a portion of the desorption effluent stream, and the regeneration inlet stream is cooled.

16. A sorptive method for recovering a chlorine-containing material from the outlet stream of a cyclic regeneration operation of a hydrocarbon conversion process using a hydrocarbon conversion catalyst, said method comprising:

- (a) passing hydrocarbons to a first catalyst bed containing a hydrocarbon conversion catalyst and converting said hydrocarbons;
- (b) passing a regeneration inlet stream comprising a first component selected from the group consisting of oxygen, hydrogen, nitrogen, and a C<sub>1</sub>-C<sub>5</sub> hydrocarbon to a second catalyst bed containing said hydrocarbon conversion catalyst, at least partially regenerating said hydrocarbon conversion catalyst in said second catalyst bed at regeneration conditions and in the presence of a chlorine-containing material, and recovering from the second catalyst bed a regeneration effluent stream comprising said material and said first component;
- (c) passing a first portion of said regeneration effluent stream to an adsorption zone containing an adsorbent, adsorbing said material on said adsorbent at adsorption conditions, and recovering an adsorption effluent

stream comprising said first component and having a reduced concentration of said material relative to said regeneration effluent stream;

5 (d) passing a desorption inlet stream comprising a second component selected from the group consisting of oxygen, hydrogen, nitrogen, and a C<sub>1</sub>-C<sub>5</sub> hydrocarbon to a desorption zone containing said adsorbent, said adsorbent in said desorption zone having said material adsorbed thereon, desorbing said material from said adsorbent in said desorption zone, and recovering a desorption effluent stream comprising said material and said second component;

10 (e) forming said regeneration inlet stream from a second portion of said regeneration effluent stream and at least a portion of said desorption effluent stream; and

15 (f) at least periodically shifting the functions of said adsorption and desorption zones by operating said adsorption zone to function as said desorption zone in (d), and operating said desorption zone to function as said adsorption zone in (c);

17. The process of Claim 16 further characterized in that the functions of said first and second catalyst beds are at least periodically shifted by operating said first catalyst bed to function as said second catalyst bed in (b), and operating said second catalyst to  
20 function as said first catalyst bed in (a).

18. The process of claim 16 wherein said hydrocarbon conversion process is a process selected from the group consisting of reforming, isomerization, and dehydrogenation.

19. The process of Claim 16 wherein said regeneration is selected from the group  
25 consisting of burning carbon deposits on said catalyst, redispersing a metal on said catalyst, adding halogen to said catalyst, drying said catalyst, and reducing a metal on said catalyst.

20. The process of Claim 16 further characterized in that at least about 80 percent of said material in said regeneration effluent stream is adsorbed on said adsorbent.

21. The process of Claim 16 further characterized in that said desorption inlet stream is formed from at least a portion of said adsorption effluent stream.

22. The process of Claim 21 wherein said first component is said second component.

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